

## A Simplified Phenomenological Theory of Viscosity for Liquid Metals

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Received July 31, 2000

This study simplifies the phenomenological theory of viscosity previously proposed by the present authors. This simplified theory has only two thermodynamic properties and one parameter, as opposed to its predecessor, which has many, allowing for easy calculation of the liquid viscosities. The viscosity of liquid metals, an excellent test for checking the validity of the liquid theory, can be calculated using the equation based on the simplified theory. The calculated results by the current theory turn out to be good for the liquid metals, including sodium, potassium, rubidium, cesium, lead and mercury.

**Keywords:** Theory of viscosity, Viscosity of liquid, Liquid metals.

### Introduction

The viscosities of liquid metals and alloys play an important role in liquid metal processing. Interest in the viscosity of liquid metals stems both from practical considerations, such as their use as atomic reactor coolants and philosophic considerations such as the fact that their structural simplicity makes them good media in which to test current theories of the liquid state. However, the high temperatures and critical contamination problems inherent in liquid metal viscometry have given rise to conflicting experimental results as well as to the anomalous viscosity dispute that has dotted the literature.

During the last 50 years various expressions for the viscosity of liquids have been presented. Representative examples are the expressions based on the statistical kinetic theory of Born and Green<sup>1</sup> and Kirkwood *et al.*,<sup>2</sup> the model theory of Frenkel,<sup>3</sup> Eyring<sup>4</sup> and Andrade,<sup>5</sup> the corresponding states theory of Helfand and Rice,<sup>6</sup> the hard sphere theory of Longuet-Higgins and Pople,<sup>7</sup> and so forth. Unfortunately, none of these expressions provides entirely satisfactory results when applied to liquid metals. A liquid metal is a severe test for any liquid theory to that extent. Low vapor pressures at melting, small differences in volume between liquid and solid, and rather large temperature ranges of the liquid state can lead to large differences between experimental and calculated values for thermodynamic properties and viscosities.

A phenomenological theory of viscosity that was proposed by the authors has been successfully applied to normal liquid,<sup>8</sup> water,<sup>9</sup> and helium,<sup>10</sup> which exhibits abnormal behavior compared to other ordinary liquids.

In the present paper, we apply the simplified expression of this theory to liquid metals adequately

### Theory

According to the previous theory of viscosity,<sup>8</sup> the viscosities of fluids through which a phonon propagates with a

velocity  $V_{ph}$  and a mean free path  $\lambda_{ph}$  can be given as follows:

$$\eta = (P_K + P_I) \lambda_{ph} / V_{ph}, \quad (1)$$

where  $P_K$  and  $P_I$  are the kinetic pressure and internal pressure of fluids, respectively.

$V_{ph}$  and  $\lambda_{ph}$  are expressed as follows:

$$V_{ph} = c_o = (\gamma / \rho \beta_T)^{1/2} \quad (2)$$

$$\lambda_{ph} = 1 / (\pi d^2 N_{ph}), \quad (3)$$

where  $c_o$ ,  $N_{ph}$ ,  $\rho$ ,  $\beta_T$ ,  $d$  and  $\gamma$ , respectively, are the velocity of sound, the phonon number density, the densities of fluids, the isothermal compressibility, the collision diameter of phonon, and the heat capacity ratio,  $C_P/C_V$ . Therefore we have

$$\eta = (P_K + P_I) \frac{(\rho \beta_T / \gamma)^{1/2}}{\pi d^2 N_{ph}}. \quad (4)$$

To calculate the viscosity, we have to know the thermodynamic properties, such as  $\rho$ ,  $P$ ,  $\alpha_P$ ,  $\beta_T$ , and  $\gamma$ . But, in general, all thermodynamic values of a fluid are not known. Therefore, we refined the above equation to reduce the data required.

The quantities on the right hand side of Eqn. (4) are intrinsic properties for the fluid in equilibrium state, therefore, we can simplify the above formula using the thermodynamic relation between them.

Eqn. (4) is reformulated as follows:

$$\eta = P_K \left( 1 + \frac{P_I}{P_K} \right) (\lambda_{ph} / c_o) \quad (5)$$

Of above equation, the ratio of  $P_K$  and  $c_o$  can be expressed as a simple form, using the following thermodynamic relationship.

$$\frac{C_P}{C_V} - 1 = \frac{TV\alpha_P^2}{C_V\beta_T} = \frac{MTc_o^2\alpha_P^2}{C_P} \quad (6)$$

And the result is as follows:

$$\frac{P_K}{c_o} = \frac{(MT)^{1/2}}{V} [C_V(1 - 1/\gamma)]^{1/2} \quad (7)$$

By introducing Eqn. (7) into Eqn. (5), we have

$$\eta_{fluid} = \frac{(MT)^{1/2}}{V} [C_V(1 - 1/\gamma)]^{1/2} \left(1 + \frac{P_I}{P_K}\right) \lambda. \quad (8)$$

In a liquid state where the intermolecular forces of neighbors are so high that the internal pressure is equal to the kinetic pressure,  $P_I \doteq P_K$ , the equation of liquid viscosity is simplified as follows:

$$\eta_{liquid} = 2 \frac{(MT)^{1/2}}{V} [C_V(1 - 1/\gamma)]^{1/2} \lambda. \quad (9)$$

### Calculations and Results

If it is assumed that the number density of the phonon is proportional to the density of molecules in the fluid, it can be expressed as

$$N_{ph} = f(N/V), \quad (10)$$

where the proportionality factor  $f$  is taken equal to the vacancy fraction in the fluid  $(V - V_s)/V$ ,  $V_s$  being the fluid volume at closest packed state.

The collision diameter,  $d$ , can be calculated using the Sutherland method<sup>11</sup> which is given by

$$d = d_o(1 + 1.8T_b/T)^{1/2}, \quad (11)$$

where  $T_b$  is the normal boiling temperature, and  $d_o$  is the values of  $d$  at infinite temperature. The parametric value  $d_o$  can be calculated from the close packed volume,  $V_s$ , and the structural information as follows:

$$d_o = (\alpha V_s/N)^{1/3}, \quad (12)$$

where  $\alpha$  is a proportionality constant that has the order of magnitude of unity and may be obtained readily for all types of regular spacings from the solid geometry of the structures. In this calculation, we take  $\alpha$  as 0.44.

The parametric values of  $V_s$  for various fluids are listed in Table 1. The only parametric value of  $V_s$  is the one obtained by fitting the calculated viscosity to the experimental data.

The calculated viscosities of sodium, potassium, rubidium, cesium, mercury and lead are listed in Table 2.

### Discussion

In spite of the practical and theoretical importance, few theories have been developed for the viscosity of liquid metals. The viscosity equation (Eqn. 9) can be applied successfully to liquid metals, an excellent check of the validity of the

**Table 2.** Comparison of Calculated and Observed Viscosities of Liquid Metals

	T/°K	$\eta_{calc.}/\mu\text{-poise}$	$\eta_{obs.}/\mu\text{-poise}$
Na	376.7	6628	6860
	440.6	4205	5040
	523.0	3308	3810
	623.0	2844	2690
	973.0	2241	1820
K	342.9	5146	5150
	440.4	3265	3310
	523.0	2760	2680
	623.0	2473	1910
	Rb	311.0	6789
320.9		6180	6258
371.7		4643	4844
413.5		4016	4133
493.1		3383	3234
Cs	316.4	6285	6299
	371.6	4555	4753
	413.5	3972	4065
	441.0	3730	3760
	483.9	3462	3430
Pb	729.0	21378	20590
	842.0	17964	17000
	976.0	15995	13490
	1117.0	14831	11850
	Hg	253.0	18379
273.0		17430	16800
293.0		16879	15500
373.0		15422	12700
473.0		14446	10100

liquid theory. To calculate the liquid viscosities by using Eqn. (9), we need the data for  $C_p$  and  $C_v$ . Since we can not find the experimental values for  $C_v$ , we can use the value of  $C_v$  from the following simple equation by Walter and Eyring<sup>12</sup> for the liquid metals.

$$C_v = 6V_s/V + 3(V - V_s) \text{ cal mole}^{-1}\text{deg}^{-1} \quad (13)$$

There may remain some arguments in using the approximations of Eqn. (10) and (11), since these equations are semi-empirical. Better approximations for  $N_{ph}$  and  $d_o$  may be available. However no adjustable parameters are involved in either equation. Although 1.8 is used in Eqn. (11), it changes slightly with the material of interest. But we chose 1.8 for the liquid metals. The calculated viscosities are in good agreement with the observed ones. If we could use the experimental values instead of the value of  $C_v$  from Eqn. (13), better calculated results would be found. Some theories of viscosity have been applied to liquid metals, but none of these provides satisfactory results from an engineering point of view. The significant structure theory, which has been used widely for many liquids, shows large deviations for liquid metals.<sup>13</sup> Notwithstanding the simplicity of this equation, we hope it may be useful for engineering applications.

**Table 1.** Parametric Values used in Calculation

	Na	K	Rb	Cs	Pb	Hg
$V_s$ (cm <sup>3</sup> /mol)	23.46	48.41	58.40	70.32	19.28	14.47

### Conclusion

Of all the current theories of viscosity, the phenomenological theory of viscosity, previously proposed by the authors, can be applied most easily to many systems with acceptable results. But they could not be used for the calculation of the viscosity of liquid metals because of the many thermodynamic properties involved. The theory is simplified as in Eqn. (9) for liquids, using the thermodynamic relations, and therefore, this theory can be used for the calculation of the viscosity of liquid metals. No adjustable parameters are involved in this equation. Through this simple viscosity equation, viscosities of liquid metals are calculated as easily as in normal liquids. The calculated and observed values are in good agreements.

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